| Q.P      | P. Code: 18ME0320  | R      | 18           |
|----------|--|--------|--------------|
| Re       | g. No:   |        |              |
|          | SIDDHARTH INSTITUTE OF ENGINEERING & TECHNOLOGY:: PUTTU  | JR     |              |
|          | (AUTONOMOUS)   |        |              |
|          | B.Tech III Year II Semester Regular Examinations July-2021<br>HEAT & MASS TRANSFER   |        |              |
|          | (Common to ME & AGE)   |        |              |
| Tim      | he: 3 hours Max.   | Marks: | 60           |
|          | $\frac{PART-A}{PART-A}$  |        |              |
| 1 0      | (Answer all the Questions $5 \ge 2 = 10$ Marks)<br>What is Fourier's law?  | T 1    | 214          |
| 1 a<br>h | What is lumped heat analysis?  | L1     | 2 IVI<br>2 M |
| c        | What is meant by laminar flow and turbulent flow?  | L1     | 2M           |
| d        | Define Boiling and Condensation.   | L1     | 2M           |
| e        | Define Radiation.  | L1     | 2M           |
|          | PART-B   |        |              |
|          | (Answer all Five Units 5 x $10 = 50$ Marks)  |        |              |
|          | UNIT-I   |        |              |
| 2 a      | Distinguish between conduction, convenction and radiation modes in heat transfer   | L3     | 5M           |
| b        | Calculate the rate of heat transfer per unit area through a copper plate 45 mm thick,  | L4     | 5M           |
|          | whose one face is maintained at 350 $^{\circ}$ C and the other face at 50 $^{\circ}$ C. Take thermal   |        |              |
|          | conductivity of copper as $370 \text{ W/m}^{-0}$ C.  |        |              |
|          | OR   |        |              |
| 3 a      | Derive the general heat conduction equation in Cartesian coordinate  | L3     | 5M           |
| b        | Derive the general heat conduction equation in Spherical coordinate.   | L3     | 5M           |
|          | UNIT-II  |        |              |
| 4 a      | Derive the expression for the overall heat transfer coefficient for a composite wall.  | L3     | 5M           |
| b        | A steel ingot (large in size) heated uniformly to 745 $^{0}$ C is hardened by quenching it in  | L4     | 5M           |
|          | an oil bath maintained at 20 $^{0}$ C. Determine the length of time required for the   |        |              |
|          | temperature to reach 595 $^{0}$ C at a depth of 12 mm. The ingot may be approximated   |        |              |
|          | as a flat plate. For steel ingot take $\alpha$ (thermal diffusivity) = 1.2×10 <sup>-5</sup> m <sup>2</sup> /s  |        |              |
|          | as a flat plate. For steel mgot take $u(merinal diffusivity) = 1.2x10^{-1}$ m /s.  |        |              |
| 5 9      | Derive an expression for heat conduction through a plane wall  | L1     | 5M           |
| b        | Explain the fin effectiveness and fin efficiency.  | L2     | 5M           |
|          | UNIT-III   |        |              |
| 6 a      | Differentiate between laminar and Turbulent flow.  | L3     | 5M           |
| b        | A cylinder body of 300 mm diameter and 1.6 m height is maintained at a constant  | L4     | 5M           |
|          | temperature of 36.5 °C. The surrounding temperature is 13.5 °C. Find out the   |        |              |
|          | amount of heat to be generated by the body per hour if $a = 1.025 \text{ kg/m}^3 = 15.06 \text{ s}$  |        |              |
|          | $10^{-6}$ $\frac{2}{10}$ $0.000$ $10^{-6}$ $\frac{2}{10}$ $0.000$ $10^{-6}$ $\frac{2}{10}$ $\frac{10^{-6}}{10}$ $\frac{10^{-6}}{1$ |        |              |
|          | 10 m/s, cp = 0.96 kJ/kg C and k = 0.0892 kJ/mh C and $\beta$ =1/298 K <sup>-</sup> . Assume  |        |              |

Nu= $0.12(Gr.Pr)^{1/3}$ .

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OR

**R18** 

A horizontal plate measuring 1.5 m x 1.1 m and at 215  $^{0}$ C, taking upward is placed in still air at 7 **10M** L4 25  $^{0}$ C. Calculate the heat loss by natural convection. The convective film coefficient for free convection is given by the following empirical relation  $h = 3.05(T_f)^{1/4}$  W/m2 0C. where T<sub>f</sub> is the mean film temperature in degree Kelvin.

## UNIT-IV

Derive the expression for Logarithmic Mean Temperature Difference (LMTD) in case of L3 8 10M counter flow.

|    | OR   |    |            |
|----|--|----|------------|
| a  | What are the applications of boiling and condensation process?               | L1 | 5M         |
| b  | Differentiate between the mechanism of film wise and drop wise condensation. | L3 | 5M         |
|    | UNIT-V   |    |            |
| Ex | Explain the surface emissive properties                                      |    | 10M        |
|    | OR   |    |            |
| De | efine Fick's law. Explain briefly.   | L1 | <b>10M</b> |

**11** Define Fick's law. Explain briefly.

\*\*\*END\*\*\*